

# **Ceramic Processing**

## **6 Green Body Formation**



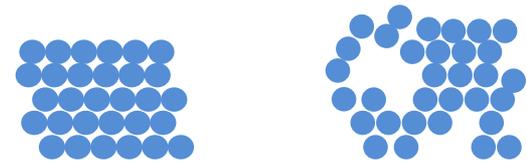
# Introduction

## □ General requirements for green body formation

Rahaman (2003), p. 328

- **Homogeneous packing of particles**

Severe variation in powder packing will lead to heterogeneity in final product microstructure and, in most cases, inferior properties (mechanical or thermal)

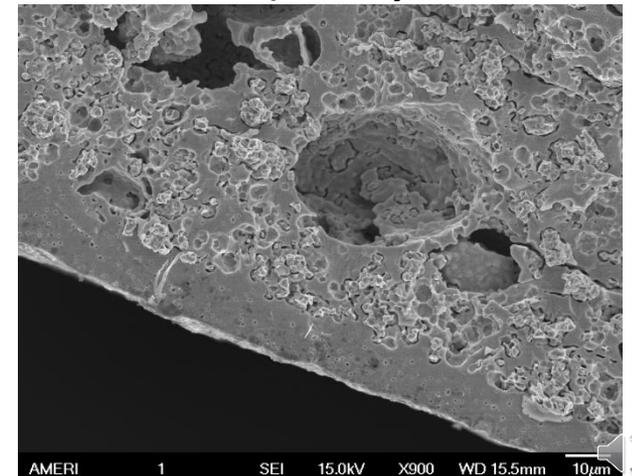


- **High packing density of particles**

Higher powder packing density leads to higher density after sintering



NiO-YSZ/YSZ bilayer co-sintered  
Cross-section (SEM by Shichen Sun)



## □ Special scenarios

- Introducing heterogeneity
  - Example: functional graded coating or electrodes
- Reducing packing density
  - Example: high porosity wanted for porous refractory or catalyst supports

# Methods for Green Body Formation (1)

## ❑ Mechanical compaction Rahaman (2003), p. 328-329

Pressing dry or semi-dry powders in metal dies with mechanical pressure (uniaxial or isostatic)

- Advantages: simplest, fast process
- Disadvantages: limited shape/dimension and microstructure uniformity

## ❑ Casting (of slurry/suspension)

Casting ceramic powder slurry/suspension with low enough viscosity that flows under its own weight

- Advantages: form complex shape
- Disadvantage: involves drying of solvent, volume shrinkage might be large

## ❑ Plastic forming

Plastically shaping thick ceramic powder paste/doll by applying mechanical stress

- Advantages: fast, continuous production
- Disadvantages: limited shape/dimension

### Dry-pressing die



<http://www.ebay.co.uk/itm/20mm-Diameter-ID-Pellet-Press-Steel-Dry-Pressing-Die-Set-Mold-/200438956668>

### Press



### Tape-casting green ceramic tape



<http://www.cgcri.res.in/page.php?id=43>  
<http://www.veniceclayartists.com/african-pottery-arts-traditional-contemporary/>

### Tape-casting green ceramic ware



### Extruded ceramic parts after sintering



[http://www.i.kts.fraunhofer.de/en/research\\_fields/processes\\_and\\_components/Shaping/Extrusion.html](http://www.i.kts.fraunhofer.de/en/research_fields/processes_and_components/Shaping/Extrusion.html)

### Extrusion of ceramic honeycomb



# Methods for Green Body Formation (2)

Forming method	Feed material	Shape of green body
Mechanical pressing		
Die compaction	Powder or free flowing granules	Small simple shape, mostly pellets or short cylinders
Isostatic pressing	Powder or free flowing granules	Large, more intricate shapes
Casting		
Slip casting	Free-flowing slurry with <b>low</b> binder content	Thin walled shape, can be intricate
Tape casting	Free-flowing slurry with <b>high</b> binder content	Thin sheets/tapes
Plastic forming		
Extrusion	Thick paste of powder and binder solution	Elongated shape with uniform cross-section
Injection molding	Granulated mixture of powder and solid binder	Small intricate shapes

Table after Rahaman (2003), p. 329

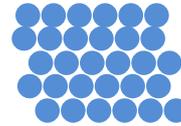


# Packing of Powders

Rahaman (2003), p. 330

## □ Models for powder packing

- **Regular (or ordered) packing**  
Mathematically simple
- **Random packing**  
More realistic



## □ Parameters used to describe powder packing

- **Packing density**

$$\text{Packing density} = \frac{V_{solid}}{V_{total}} = \frac{V_{solid}}{V_{solid} + V_{space}}$$

- **Apparent volume (or relative bulk volume)**

$$\text{Apparent volume } V_a = \frac{V_{solid} + V_{space}}{V_{solid}} = \frac{1}{\text{Packing density}}$$

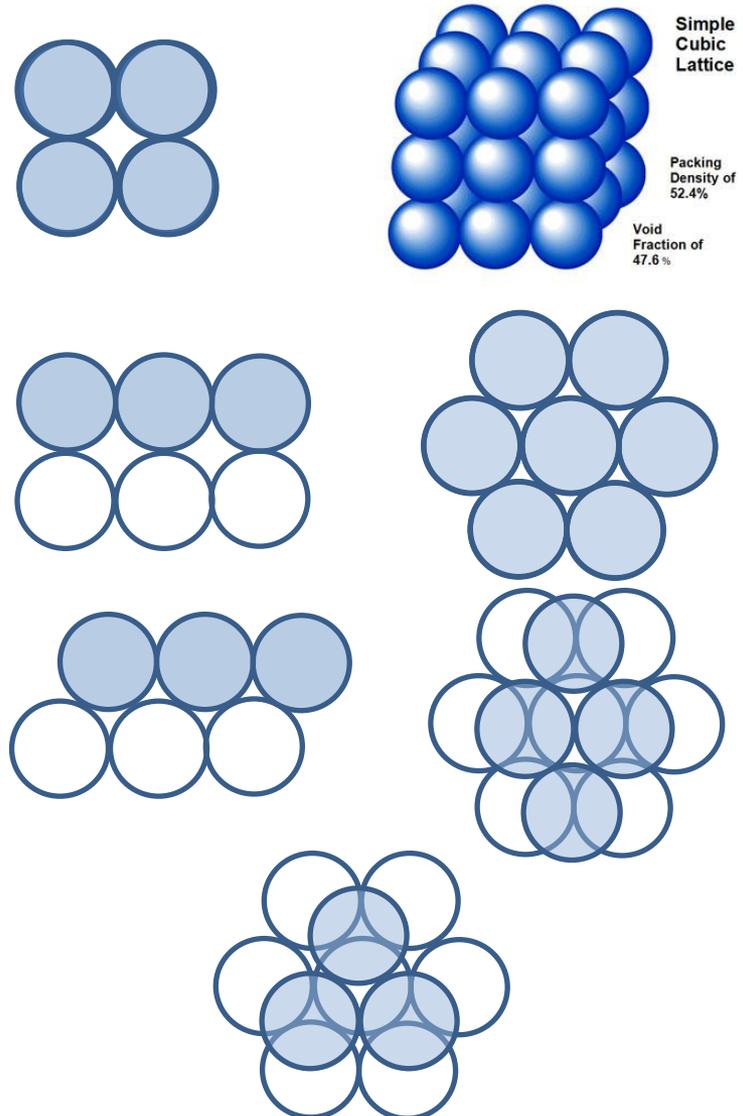
- **Coordination number (CN)**

The number of particles that are in direct contact with a particular particle

# Regular Packing of Monosized Spheres

## □ Examples of regular packing

- Simple cubic
  - CN = 6
  - Packing density  $\frac{\pi}{6} \approx 52.4\%$
- Simple hexagonal
  - CN = 8 (or 6 + 1 + 1)
  - Packing density  $\frac{\pi}{3\sqrt{3}} \approx 60.5\%$
- Tetragonal-sphenoidal
  - CN = 10 (or 6 + 2 + 2)
  - Packing density  $\frac{2\pi}{9} \approx 69.8\%$
- Rhombohedral (like FCC or HCP)
  - CN = 12 (or 6 + 3 + 3)
  - Packing density  $\frac{\pi}{3\sqrt{2}} \approx 74.0\%$



# Random Packing of Particles

## ❑ Loose random packing

Powders are loaded into a container and are not allowed to re-arrange to as favorable state as possible

- This gives the so-called poured density or freely settled density

## ❑ Dense random packing

Powders are loaded into a container and vibrated or tapped to reach a state of highest packing density

- This gives the so-called tap density



Rahaman (2003), p. 331-332

<http://www.quantachrome.com/density/autotap.html>

# Random Packing of Monosized Particles

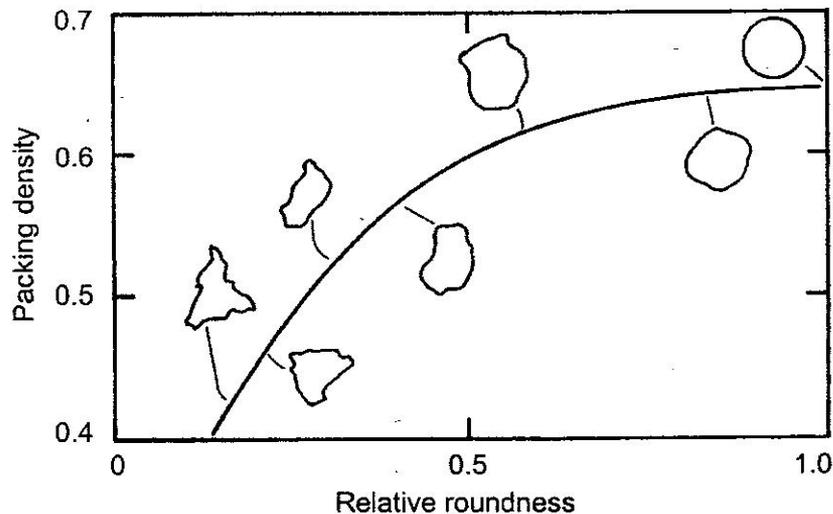
## □ For mono-sized spheres

Rahaman (2003), p. 332-334

- Relative density upper limit of random packing of monosized spheres is ~64%
- Loose random packing gives packing density of ~57-61%
- The non-uniformity is local and, often small beyond 3 sphere diameter

## □ Practical systems

- Particles deviate from spheres and the further it is away from sphere or equiaxial shape, often the lower the packing density
- Anisotropic particles (e.g., needles or plates) usually give low packing density; but if there is preferred orientation/ordering, packing high density can be high

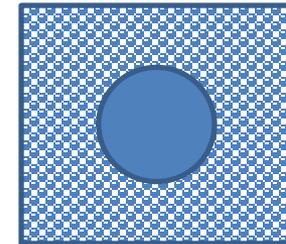
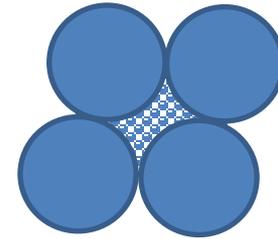


Particle shape	Aspect ratio	Packing density
Sphere	1	0.64
Cube	1	0.75
Rectangle	2:5:10	0.51
Plate	1:4:4	0.67
Plate	1:8:8	0.59
Cylinder	5	0.52
Cylinder	15	0.28
Cylinder	60	0.09
Disk	0.5	0.63
Tetrahedron	1	0.5

# Random Packing of Bimodal Sized Spheres

## □ Packing density could improve for bimodal spheres compared with monosized spheres

- For large particles → filling of interstitials between large spheres with smaller particles gives higher packing density
- For small particles → replacing of regions of small spheres packing with large, dense particles also gives higher packing density

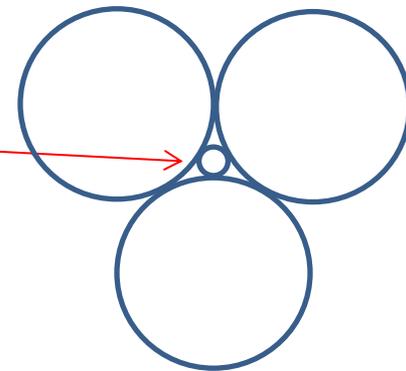
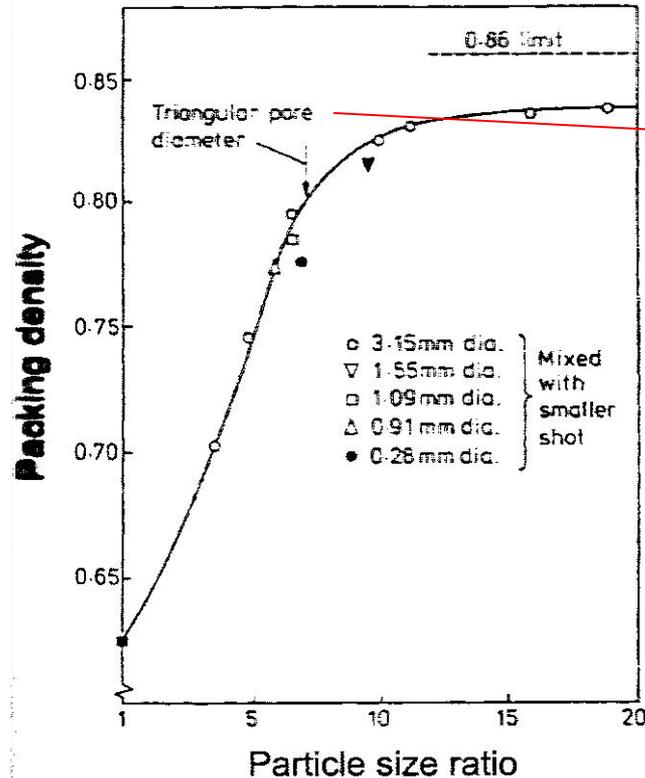
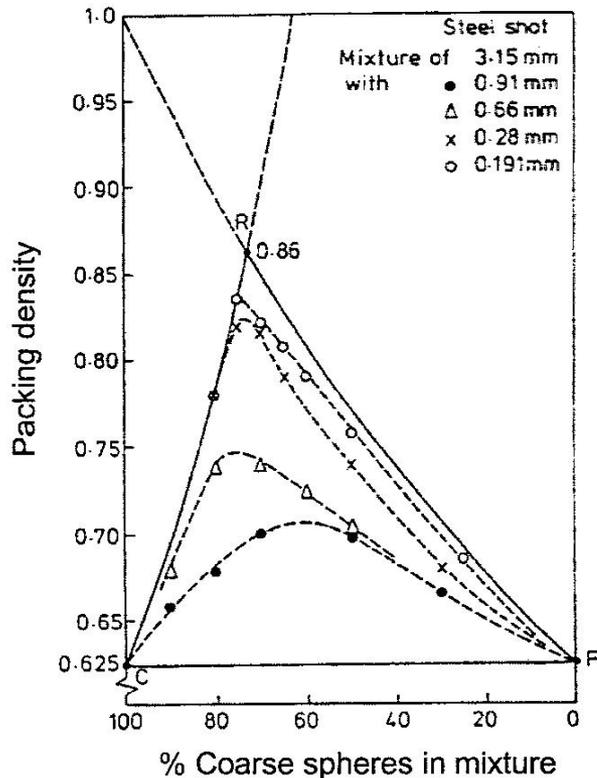


## □ The packing density for bimodal sized spheres is a function of

- Ratio of sphere diameters
- Fraction of large (or small) spheres

# Size and Fraction Effect on Random Packing of Biomodal Sized Spheres

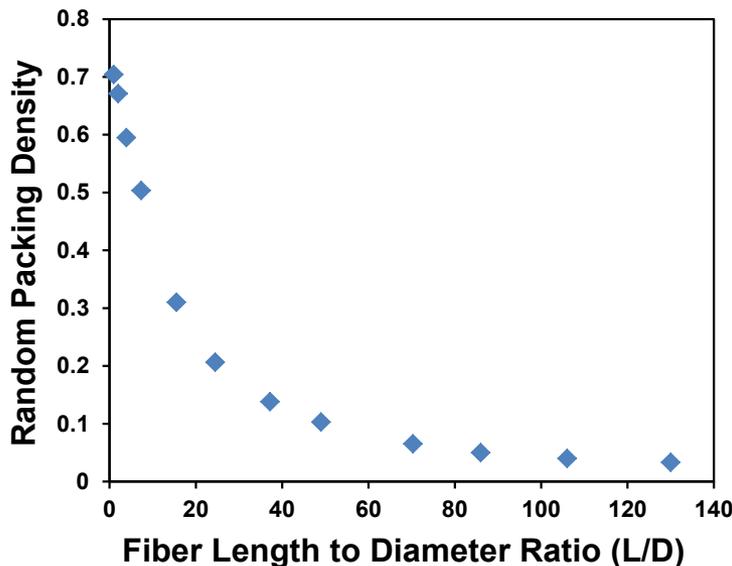
- ❑ For the same size ratio, at intermediate weight fraction for large particles equals  $\sim 0.733$ , the dense random packing density reaches highest, which, theoretically could reach  $\sim 0.86$
- ❑ Dense random packing density increases as particle size ratio increases, reaching plateau at size ratio of  $\sim 15$



Rahaman (2003),  
p. 334-337  
Plots original data from  
McGeary, J Am Ceram  
Soc, 1961 vol. 44, p513

# Random Packing of Bimodal Sized Nonspherical Particles

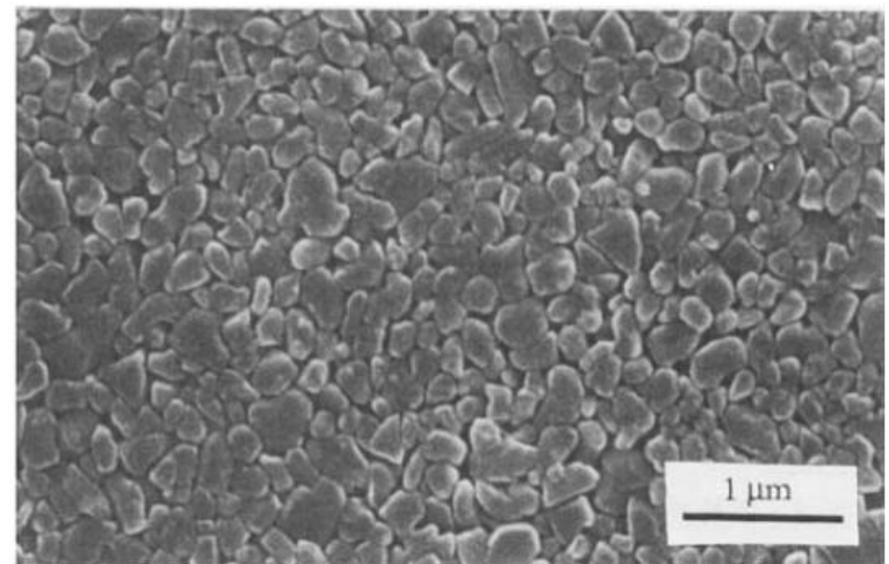
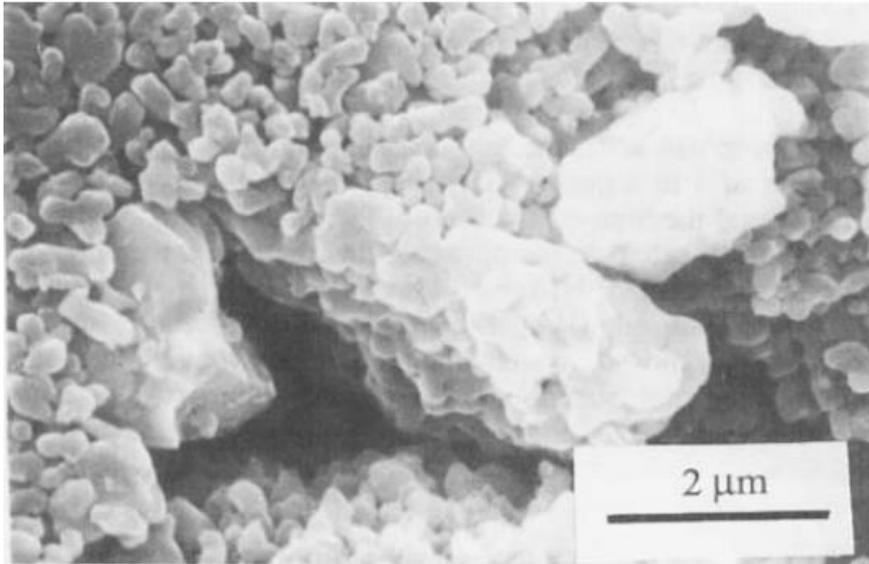
- ❑ Similar to spheres, random packing of bimodal sized non-spherical particles also leads to increased packing density
- ❑ Packing density generally depends on
  - **Size ratio** between two modes of particles
  - Weight or volume **fraction** of larger vs. smaller particles
  - Particle **shape**
    - E.g.: fibers/whiskers give low packing density and it gets worse as whisker length to diameter aspect ratio increase → generally whiskers L/D ratio kept in range of 15-20



Whisker		Particle Dia. /Whisker D ratio				
L/D	Vol.%	0	0.11	0.94	14.30	$\infty$
3.91	25	68.5	68.5	61.7	74.6	82.0
3.91	50	76.4	74.6	61.7	72.5	75.9
15.52	25	68.5	66.7	59.9	54.1	65.0
15.52	50	61.7	55.6	50.7	44.3	48.1
37.10	25	50.0	48.0	42.0	33.1	41.3
37.10	50	25.7			22.6	25.6

# Random Packing of Particles with Continuous Size Distribution

- ❑ Practical powders have continuous size distribution
- ❑ Particles with continuous size distribution could, in principle, pack to very high density.
  - Normally, the wider the distribution, the higher the density
- ❑ Draw backs of using powders with very wide size distribution: possibility of non-uniformity in green body and defects in sintering



Rahaman (2003), 341-344; Figures from Roosen, J Am Ceram Soc, 1988 vol. 71, p970

# Mechanical Compaction

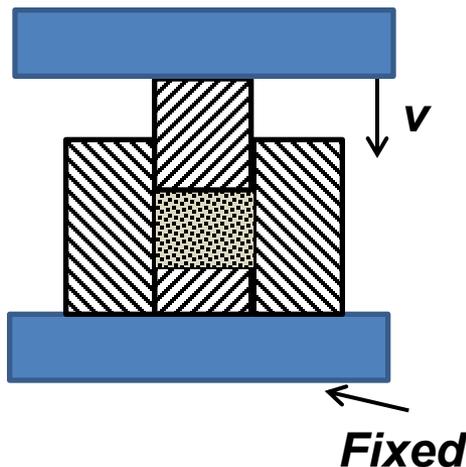
## □ General features

- Moisture content in powders for dry and semi-dry pressing
  - < 2 wt% of water for dry pressing
  - < 5-20 wt.% for semidry pressing

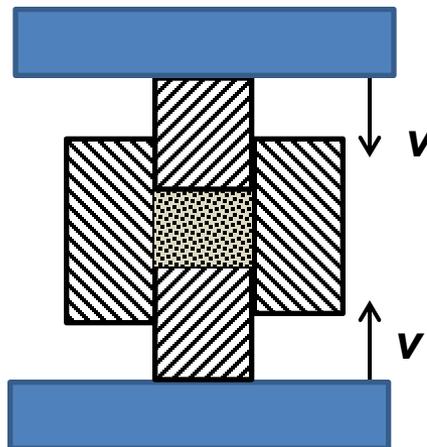
## □ Die compaction

- Used for simple shapes – mostly disks and short cylinders
- Modes of operation:

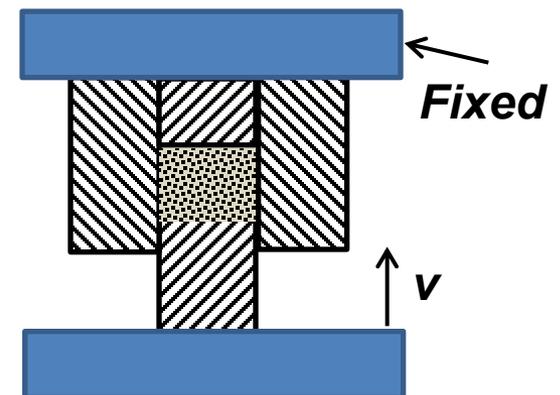
### Single action mode



### Dual action mode



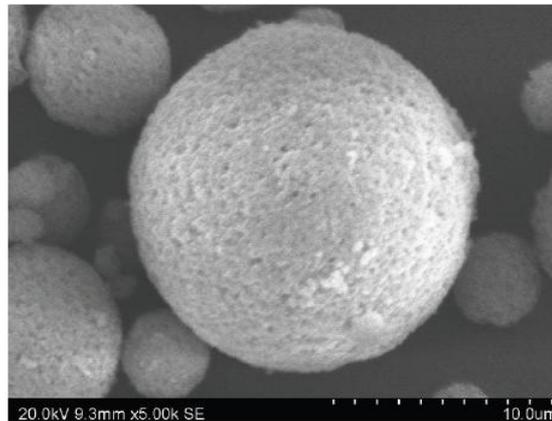
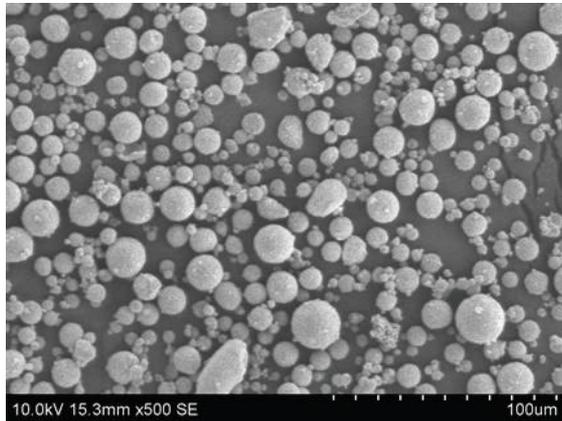
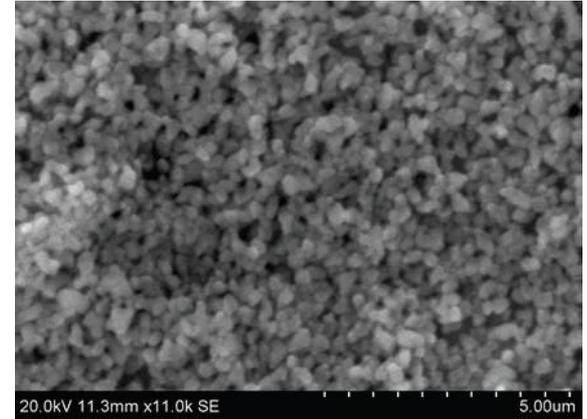
### Floating mode



# Powders & Granules for Die Filling

## □ Powders used

- Fine powders
  - OK for lab, but poor flowability for industrial production
- Granules (e.g., made by spray drying)
  - Size often  $\sim 10\text{-}400\ \mu\text{m}$
  - Improves flow capability
  - Often contain additives (e.g., PVA binder)



Abhisek Choudhary,  
ISRN Ceramics, 2013,  
264194

## □ Die filling density: $\sim 20\text{-}35\%$

Packing density of  $\sim 45\text{-}55\%$  within each granule and  $\sim 60\%$  for packing of granules

# Die Compaction – Primary Particles vs. Granules/Agglomerates

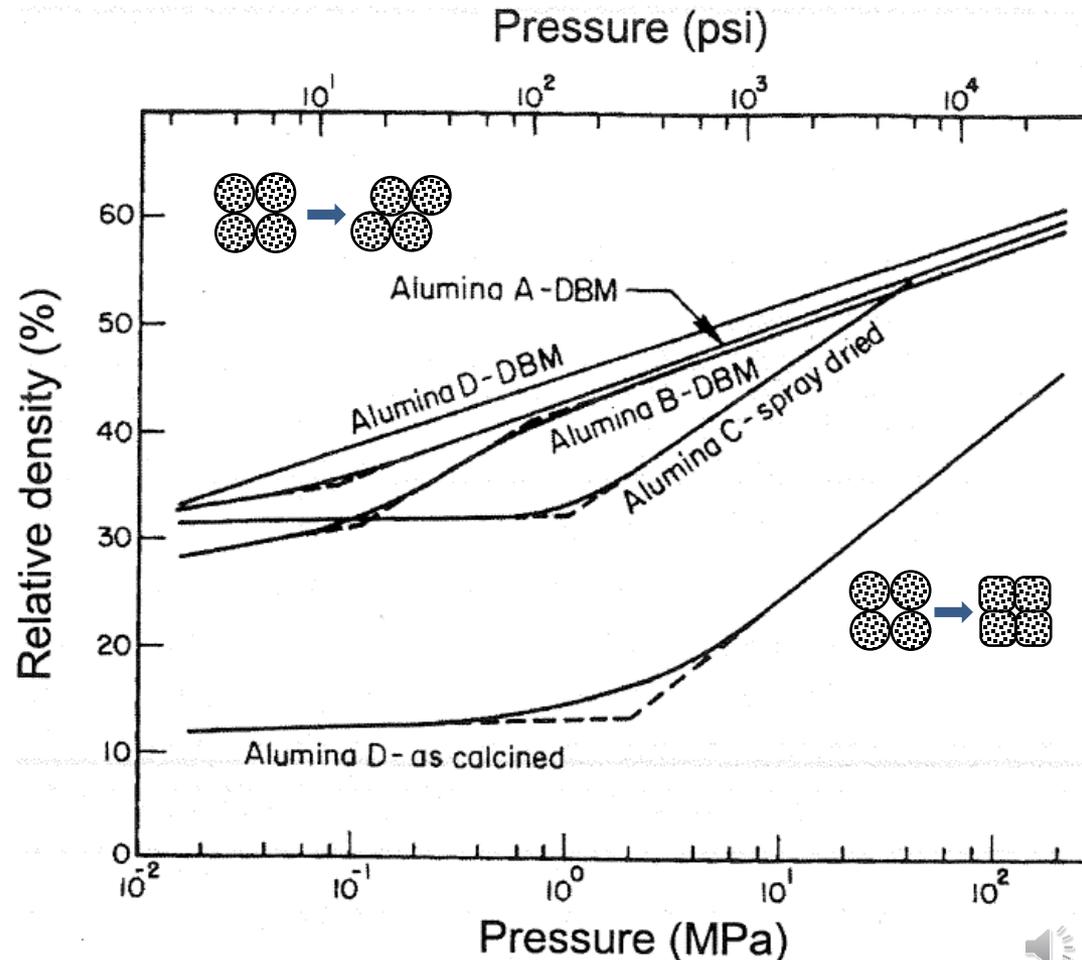
## □ One-stage compaction for primary particles

- Packing density increases directly with pressure due to re-arrangements and fractures at higher pressure

## □ Two-stage compaction for large granules/agglomerates

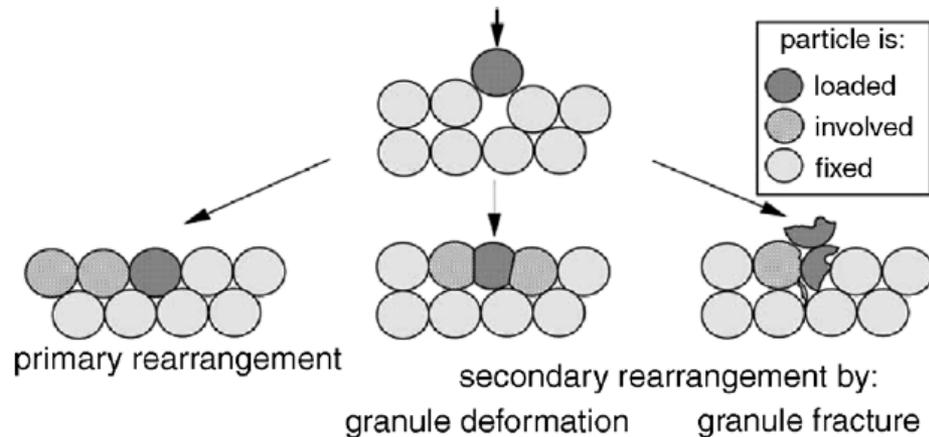
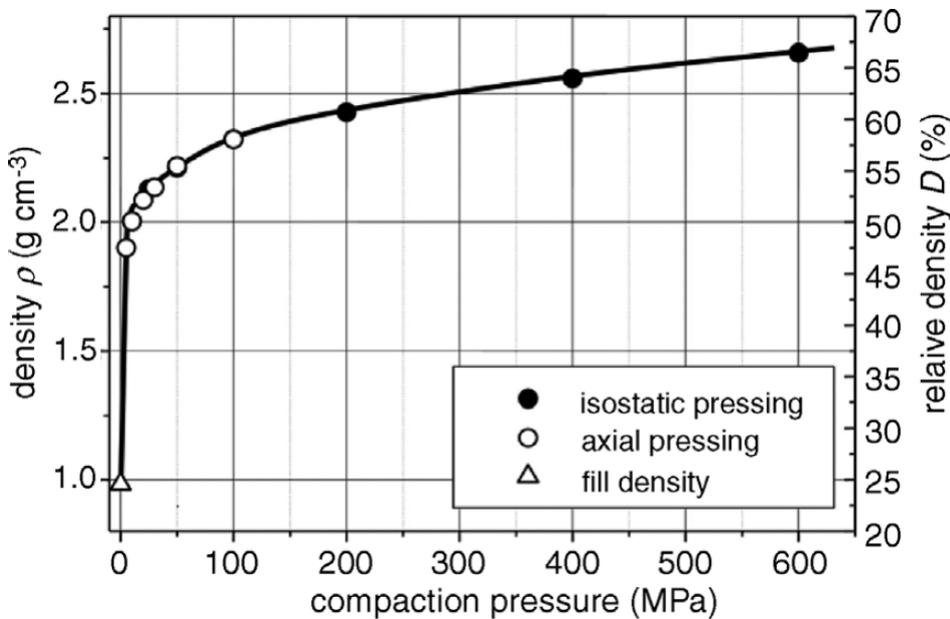
- Low pressure: packing density increases very slowly
  - Reduction of large voids by rearrangement of granules
- Higher pressure: packing density increases more rapidly
  - Deformation and fragmentation of granules

Rahaman (2003), 362-371; Figure from Niesz, D E et al. Mater Sci Research: Processing of Crystalline Ceramics; , v 11, 1978 p. 41



# Die Compaction – Pressure Effects: Rearrangement, Deformation, & Fracture

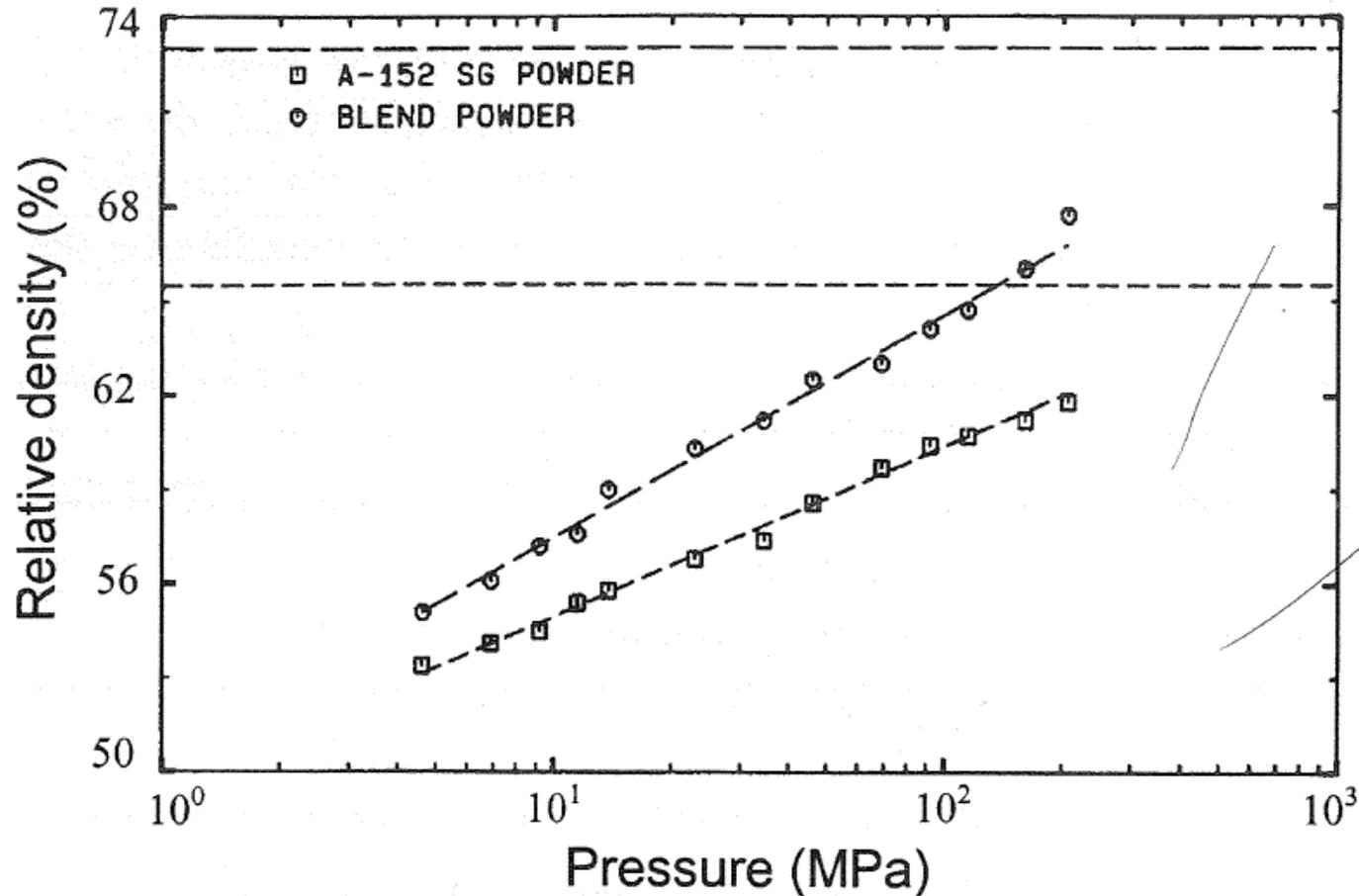
- Generally, higher pressure leads to higher packing density, but saturates at ~random close packing density
- Different processes occur as pressure is applied including re-arrangement, deformation, and fracture



Rahaman (2003), 362-371; Figures credit of R Roberacker, Powder Compaction by Pressing, in Ceramics Science and Technology, Volume 3, Synthesis and Processing, 2012, p. 1-37

# Die Compaction – Powder/Granule Size Distribution Effect

- Wider granule (or powder) size distribution (e.g., via blending) gives higher density

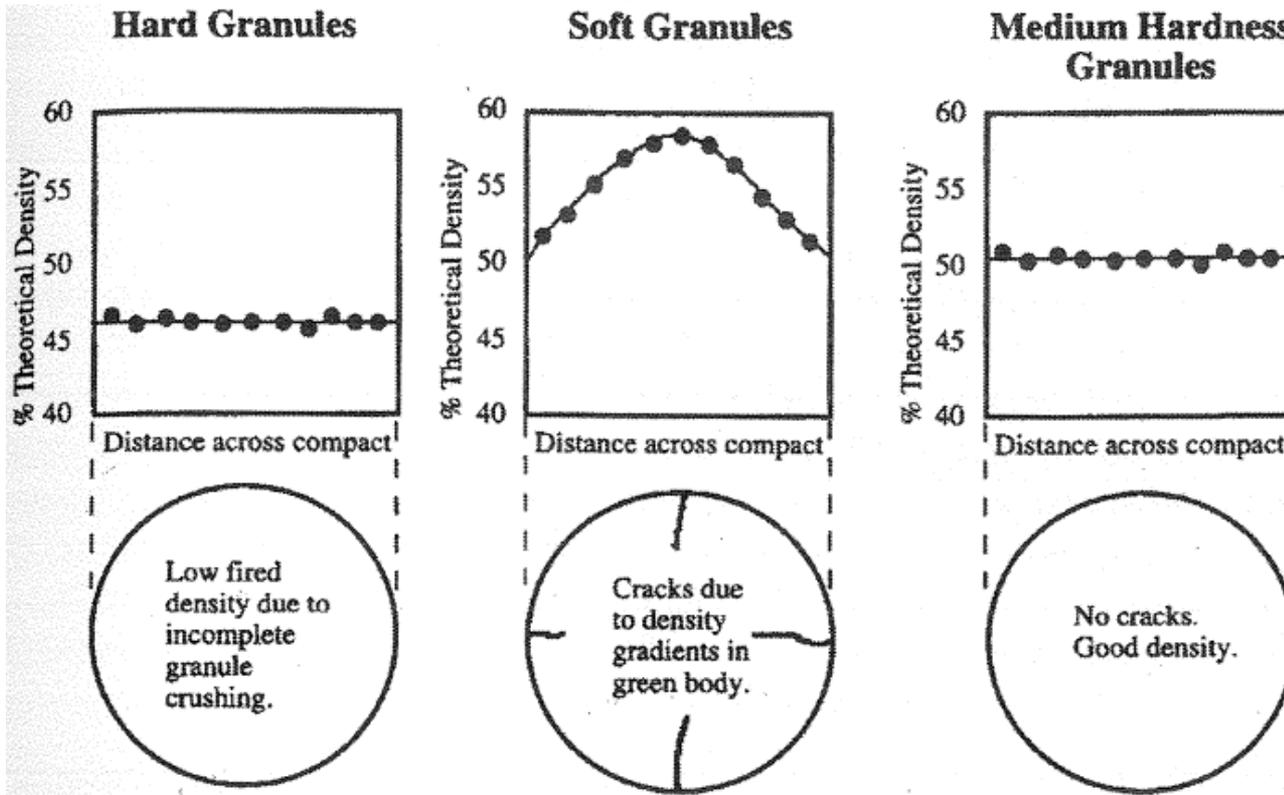


Rahaman (2003), 362-371; Figures credit of R. Zheng, J. Am. Ceram. Soc. 1988, Vol. 71, p. C456

# Die Compaction – Granule Hardness Effect (1)

## □ Granule hardness effect

- Too **hard** granules give low packing density due to intergranules pores
- Too **soft** granules give high packing density but possibly severe non-uniformity
- Medium hardness granules give high packing density and good uniformity

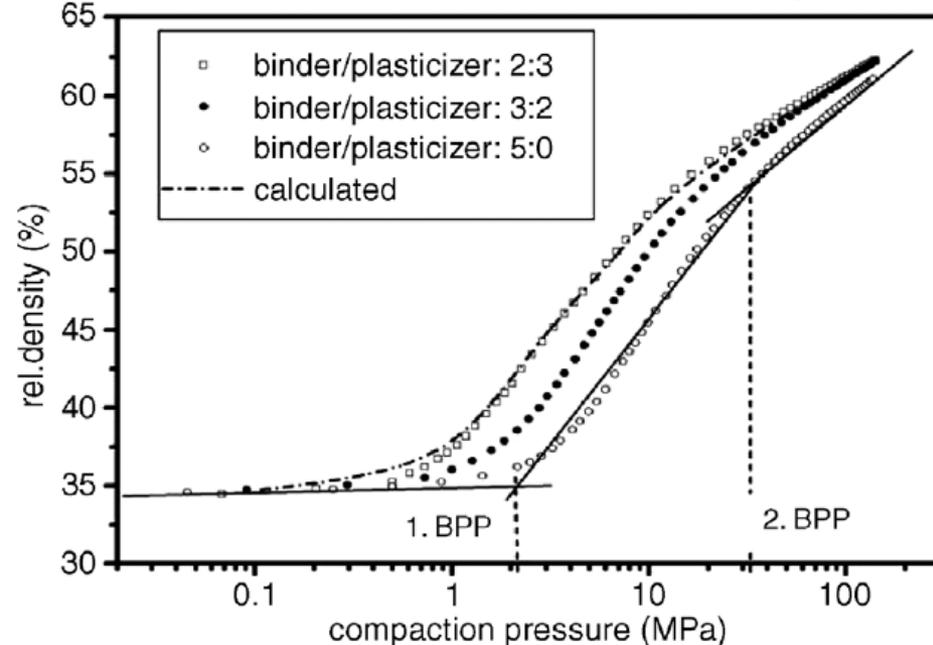
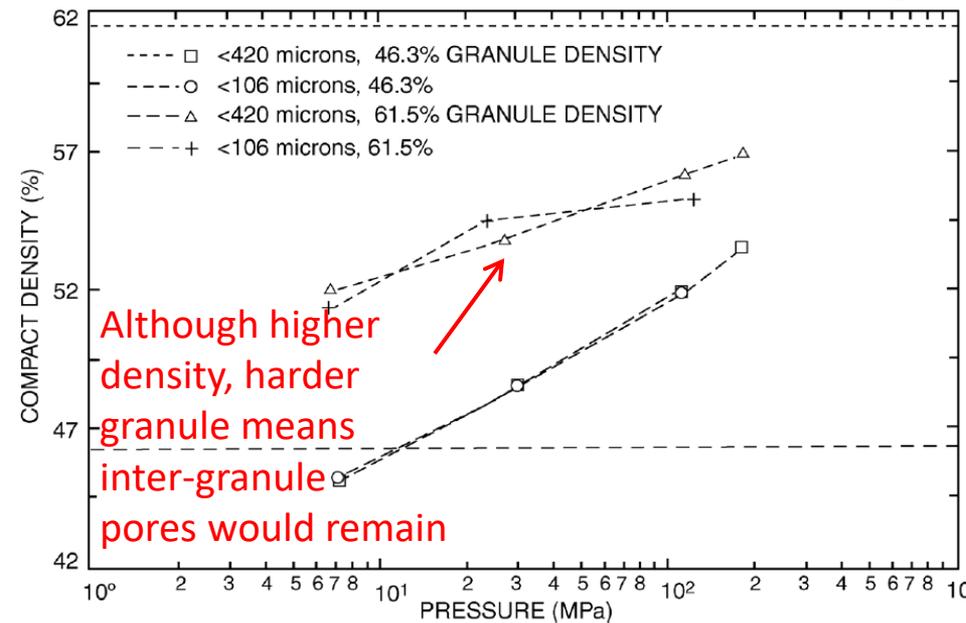


Rahaman (2003), 362-371; Figure credit of Glass SJ, MRS Bulletin, 1997 Vol. 22 (12), p. 24

# Die Compaction – Granule Hardness Effect (2)

## □ Granule hardness can be changed by

- Controlling dispersion of powders, e.g., use of partially flocculated slurry instead of fully stable colloidal slurry
- Using polymer binder with lower  $T_g$  or adding (more) plasticizer to reduce  $T_g$

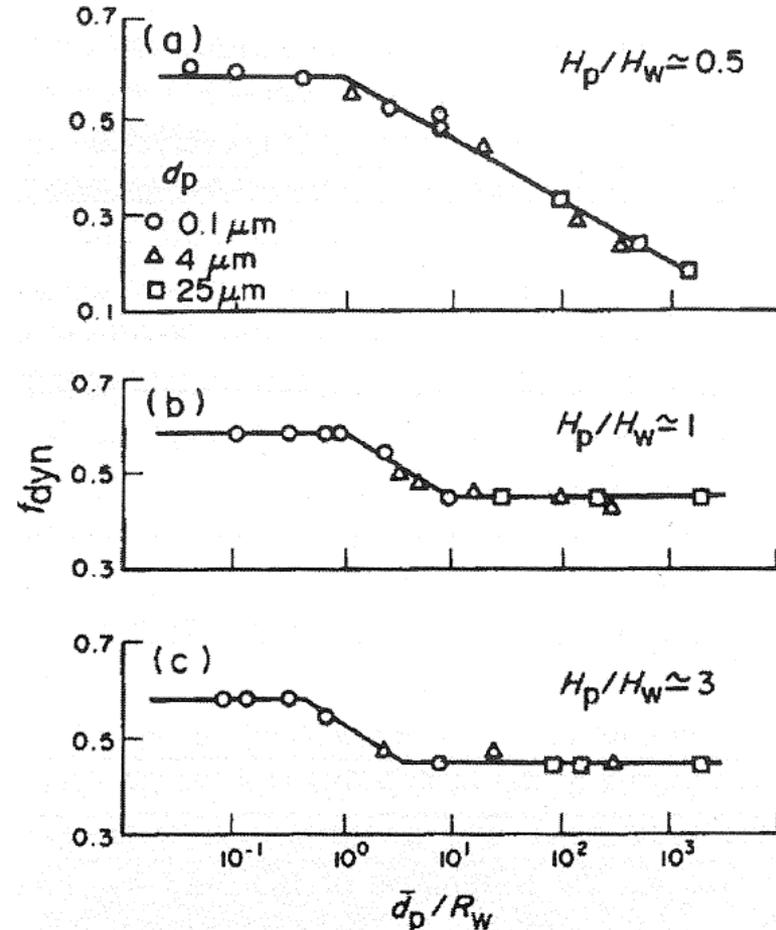
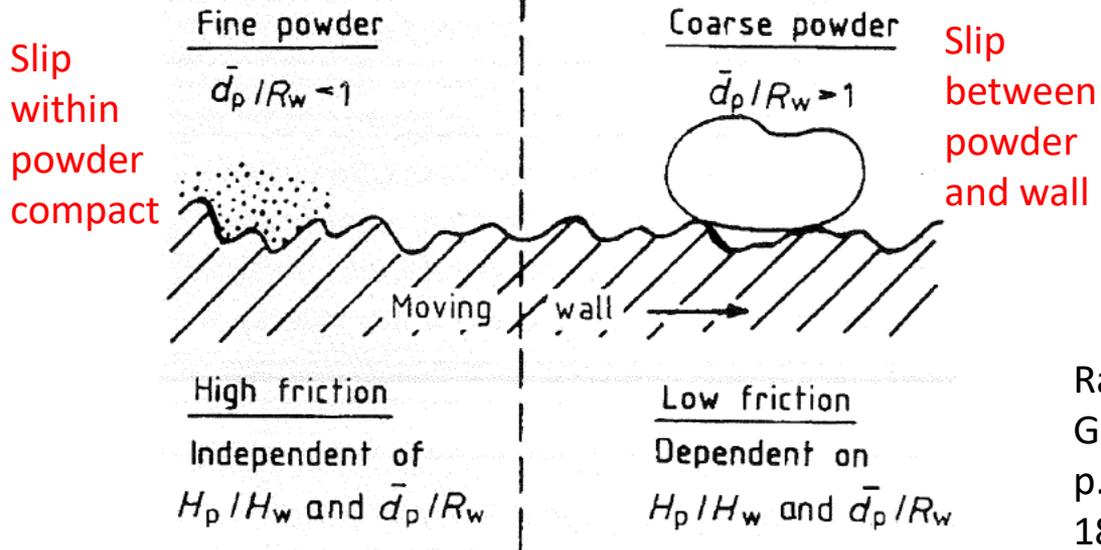


Rahaman (2003), 362-371; Figures credit of R. Zheng, J. Am. Ceram. Soc. 1988, Vol. 71, p. C456 and Agniel, Y. (1993) Bedeutung der Einzelgranalieneigenschaften zur Defektvermeidung in trockengepressten keramischen Modellpulvern. Ph.D. dissertation, Universität Karlsruhe, 1992, Institute for Ceramics in Mechanical Engineering IKM 009

# Die Compaction – Die and Powder Interaction Effects

## Factors influencing powder compaction

- Particle size  $\bar{d}_p$  vs. die wall roughness  $R_w$ 
  - Rougher the die wall or smaller the particles, higher the friction coefficient until plateauing
- Hardness of particles  $H_p$  vs. die wall  $H_w$ 
  - Harder the die wall, lower the friction coefficient
- Direction of grooves on die wall
- Lubricant
  - More effective for finer powders



Rahaman (2003), 362-371; Figures credit of van Groenou, Powder Metallurgy Int, 1978, vol. 10, p.206 and Strijbos S. Powder Technol, 1977, vol. 18, p.209

# Release of Powder Compact after Pressing

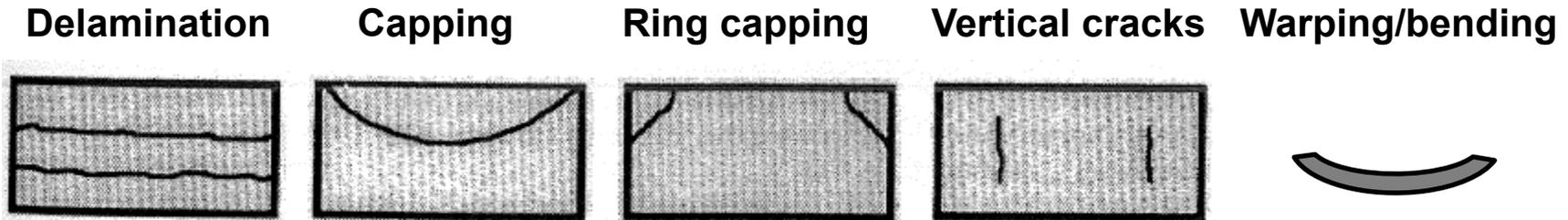
## □ Phenomena of “Spring back”/Strain recovery

- After applied pressure is released, powder compact expands slightly and releases stored elastic energy
- Features
  - Generally more significant for higher pressure and/or higher organic contents
  - May increase friction between powder compact and sample and also cause damage to the sample
  - Lubricants (e.g., stearic acid) could help reduce friction and reduce pressure for ejection



# Defects in Pressing

## □ Defects



- Origins: pressure and/or density variation due to internal/wall frictions and inhomogeneous die filling

## □ Approaches to mitigate defects

- Ensure uniform die filling: use powder with good flow capability and uniformity
- Use organic binder
  - Increase compact strength
- Use lubricants
  - Reduces friction with wall and between particles
  - Decrease pressure needed and spring back
- Use small thickness to diameter ratio  $t/D$ 
  - generally  $<0.5$  for single action  $<1$  for double action

# Isostatic Pressing

❑ Use of fluid to transfer pressure in pressing process

❑ Advantages

- Uniform pressure
- Higher pressure allowable

❑ Wet bag isostatic pressing

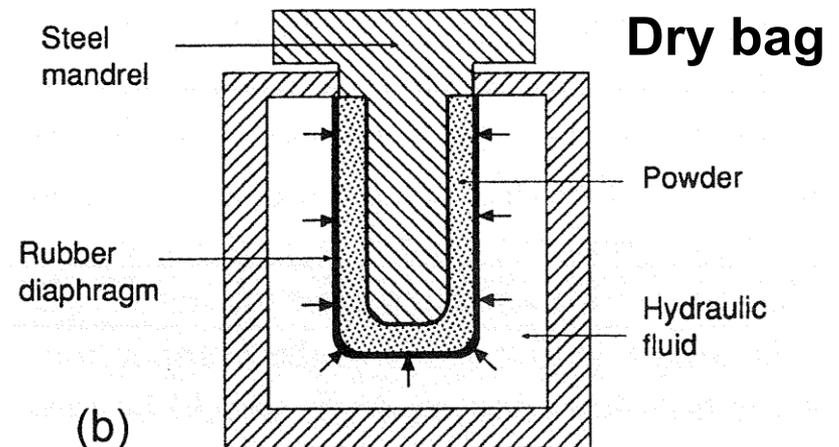
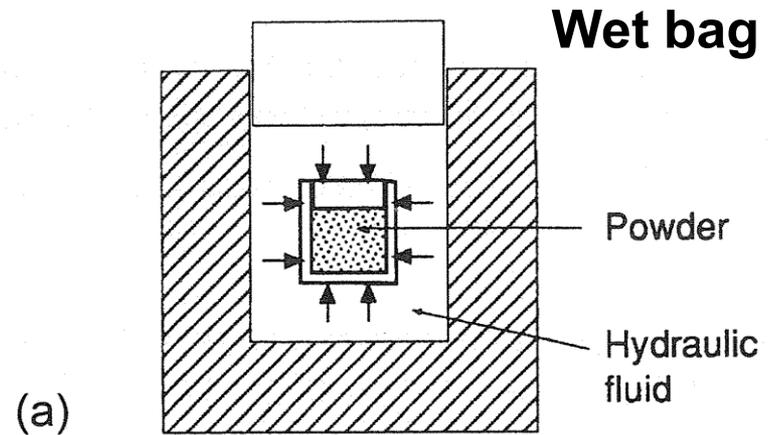
Pre-shape the sample, load in soft bag, (vacuum) and immerse in hydraulic fluid, apply high pressure

- Used for complex shape and large size sample

❑ Dry bag isostatic pressing

Load powder in thick rubber bag, with rigid core or support, then apply pressure

- Easier for automation and used for small sample or simple shape



# Casting

## □ Casting

Casting ceramic powder slurry/suspension with low enough viscosity that flows under its own weight, followed by removal of liquid that leads to consolidation of powders

## □ General requirements

- Homogeneous particle packing
- Green density as high as possible → High particle content in slurry
- Reasonable rheology → Not too high particle content in slurry

## □ Advantages

- Low cost process capable of making complex (thin walled) shapes or thin sheets

## □ Major categories

- Slip casting
- Tape casting
- Pressure casting
- Gel casting
- Electrophoretic deposition

Rahaman (2003), 362-371

# Slip Casting (1)

## □ Process description

Slurry (slip) is poured into porous mold, which sucks solvent (e.g., water) away by capillary force

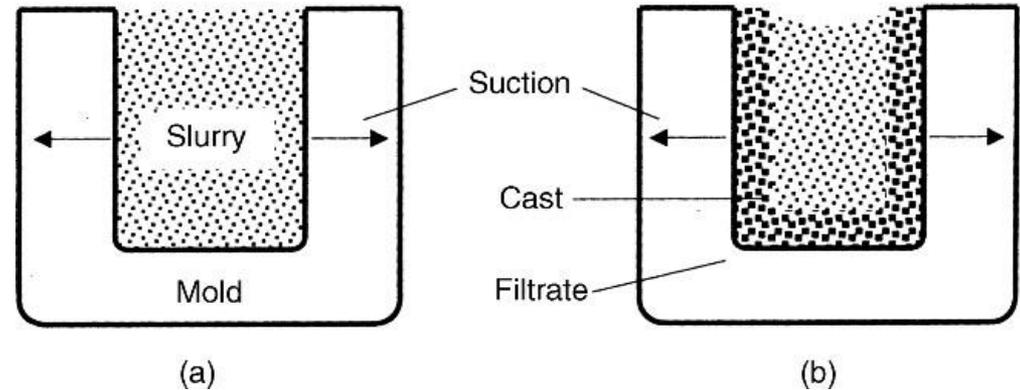
## □ General slip casting mechanism

- Darcy's law

Solvent flux  $J$

$$J = \frac{K}{\eta_L} \cdot \frac{dp}{dx}$$

- $K$  Permeability of the porous medium (consolidated layer and porous mold)
- $\eta_L$  Solvent viscosity
- $dp/dx$  Pressure gradient



# Slip Casting (2)

□ Thickness of cast  $L_c$  increases with time following parabolic law

$$L_c^2 = \frac{2K_c p}{\eta_L (V_c / V_s - 1)} t$$

$K_c$  Permeability for the consolidated cast body

$p$  Pressure difference across the cast body

$\eta_L$  Solvent viscosity

$V_c$  Volume fraction of solid in the cast body

$V_s$  Volume fraction of solid in the slurry

## Implications:

- Cast thickness growth rate decreases with time (or cast thickness)
- Optimal pore size in mold for compromise between  $p$  and  $K_c$
- Slurry should be **partially stabilized** to prevent too dense cast (which gives too low permeability) and too loose cast (which gives non-uniform microstructure)
- Increasing solid content or decreasing viscosity (e.g., via increasing temperature) lead to increased cast thickness growth rate

# Tape Casting

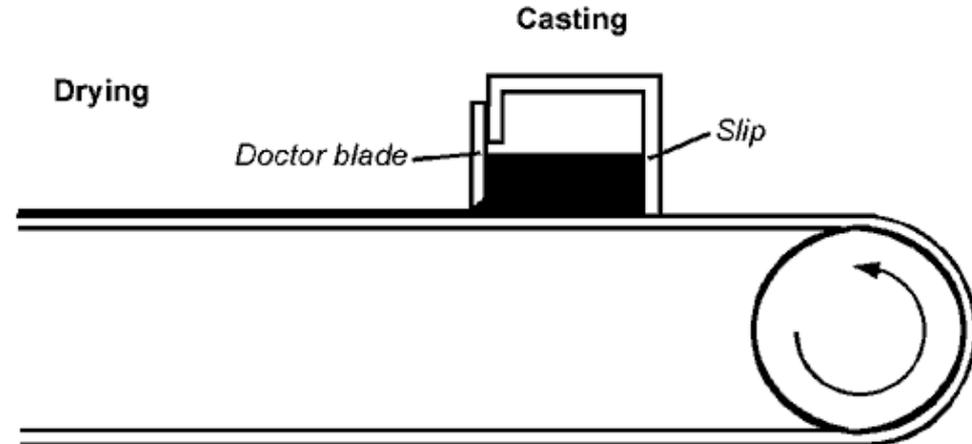
❑ **Slurry cast onto carrying tape with thickness controlled by the gap between blade and tape**

❑ **Use**

For production of film/tapes with thickness  $\sim 10\text{-}1000\ \mu\text{m}$

❑ **Slurry formulation considerations**

- Solvents:
  - Usually organic: Acetone or MEK for thin tapes and Toluene for thicker tapes ( $>0.25\ \text{mm}$ )
  - Aqueous solvent getting more common: see Hotza and Greil, Mater Sci & Eng: A Vol202 (1-2), 1995, p 206
- Ceramics: 30-80 wt%
- Binder:  $\sim 1\text{-}5\ \text{wt}\%$  ( $\sim 2\text{-}30\ \text{vol}\%$ )
- Plasticizer: 1-3 wt%
- Dispersant:  $<\sim 1\ \text{wt}\%$

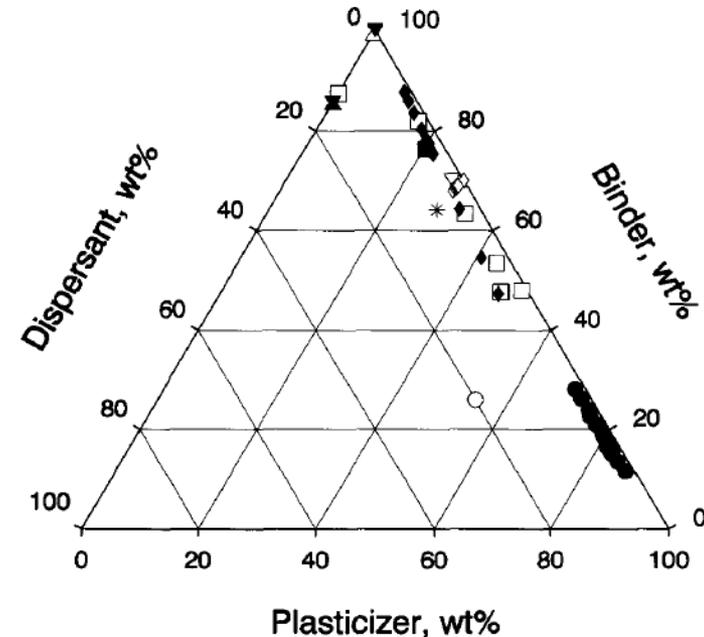
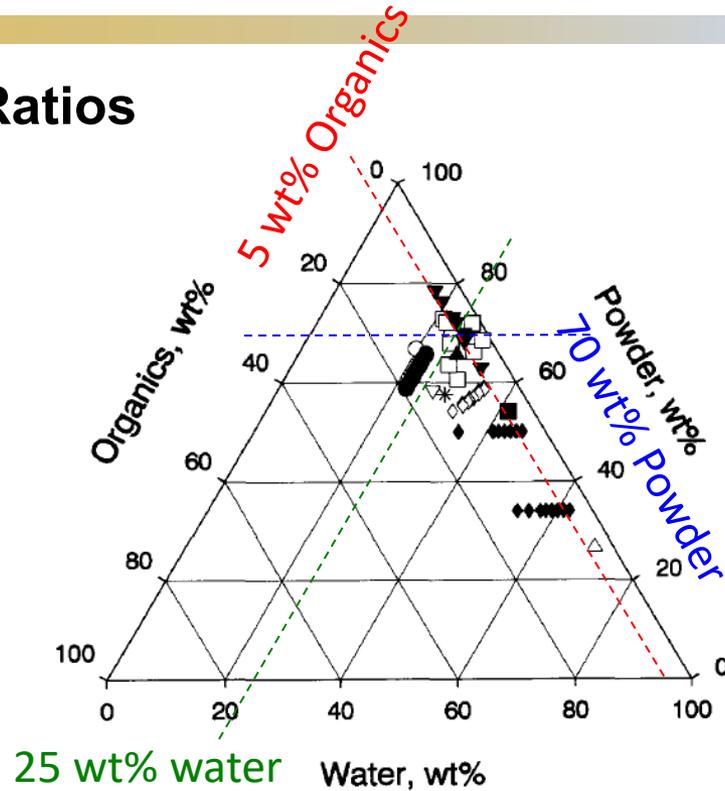


<http://www.keramverband.de/pic/ebild57.gif>

Rahaman (2003), 372-391

# Tape Casting - Aqueous System Formulation

## □ Ratios



## □ Examples:

- Binder: PVA, PAA, PVAc,  $\text{NH}_4\text{PA}$ , cellulose ether, acrylic polymer and co-polymer
- Plasticizer: PEG, glycerol, PPG
- Dispersant: polyelectrolytes such as acryl sulfonic acid,  $\text{NH}_4\text{PMA}$ ,  $\text{NH}_4\text{PA}$

See Hotza and Greil, Mater Sci & Eng: A Vol202 (1-2), 1995, p 206

# Other Casting-Based Techniques

## □ Pressure casting

- Applying pressure in casting process
- Advantage: faster consolidation/solvent removal

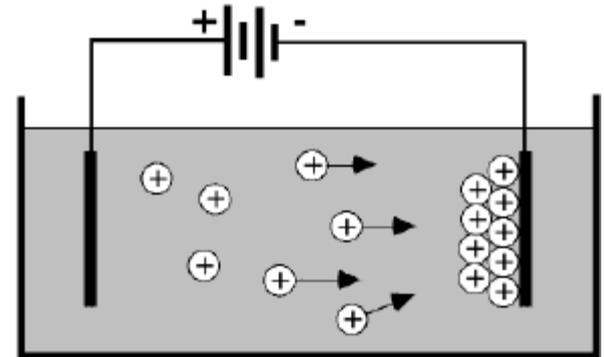
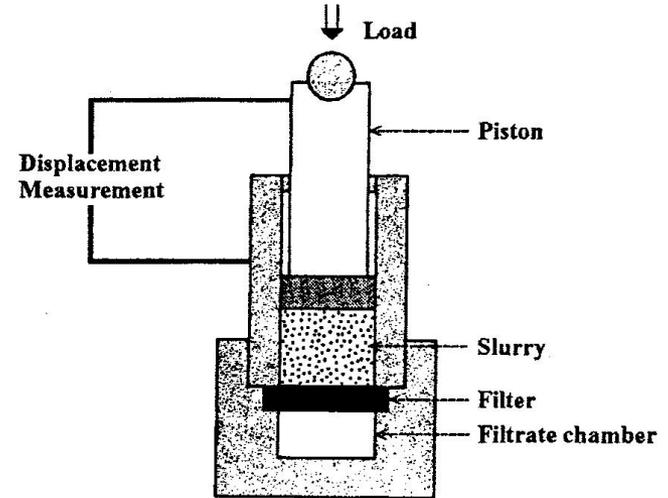
## □ Gel casting

- Add organic monomer to cast slurry, which undergoes gelation (polymerization) process and prevents particle settling or segregation and also strengthen the body to withstand capillary stress during drying.
- Advantage: thicker green body with low polymer content for easier burn out`

## □ Electrophoretic deposition

- Depositing green body from stable colloidal suspension via electrophoresis
- Advantage: better controllability

□ **Disadvantages:** more complex/higher cost



Rahaman (2003), 372-391;  
[http://www.vtscience.com/EPD\\_Pages/What\\_is\\_EPD.html](http://www.vtscience.com/EPD_Pages/What_is_EPD.html)

# Plastic Forming

❑ Forming ceramic green body from moldable or plastic powder-additive mixtures

❑ Major categories

- Injection molding
- Extrusion

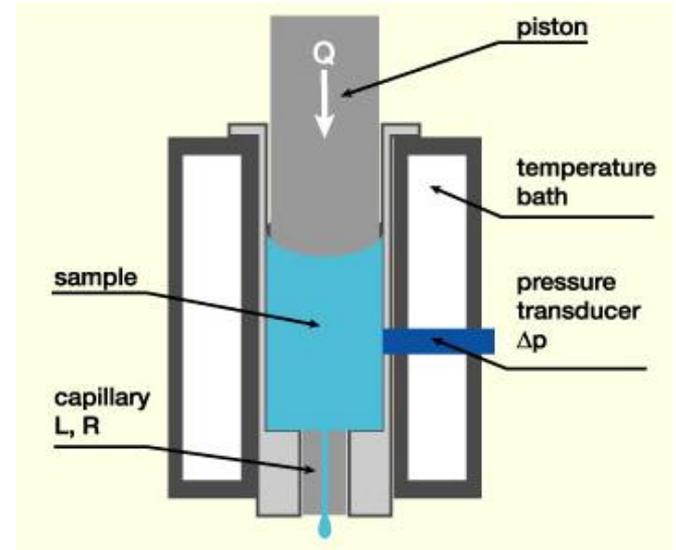
❑ Basic requirements of ceramic paste

- Moldable - plastic deformation above certain stress level
- Ability to withstand deformation under own weight

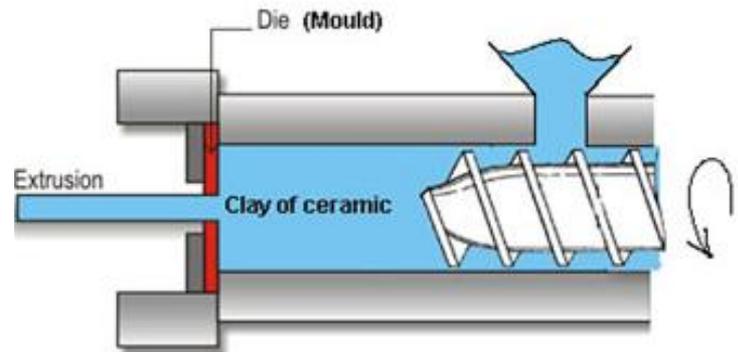
❑ Extrusion instrument

- Piston type
- Screw type

Rahaman (2003), 391-399



<http://www.adhesivesmag.com/articles/85163-tailoring-psa-dispersion-rheology-for-high-speed-coating>



[http://www.dsource.in/course/ceramics-II/plastic\\_state\\_forming\(extrusion-pressing\)/index.html](http://www.dsource.in/course/ceramics-II/plastic_state_forming(extrusion-pressing)/index.html)

# Extrusion Formulation

## ❑ Manipulating plastic behavior of feed material

- For clay: powder water interaction
- For technical ceramics: addition of organic binder, usually high molecular weight binder polymer such as methyl cellulose, polyacrylimides, PVA

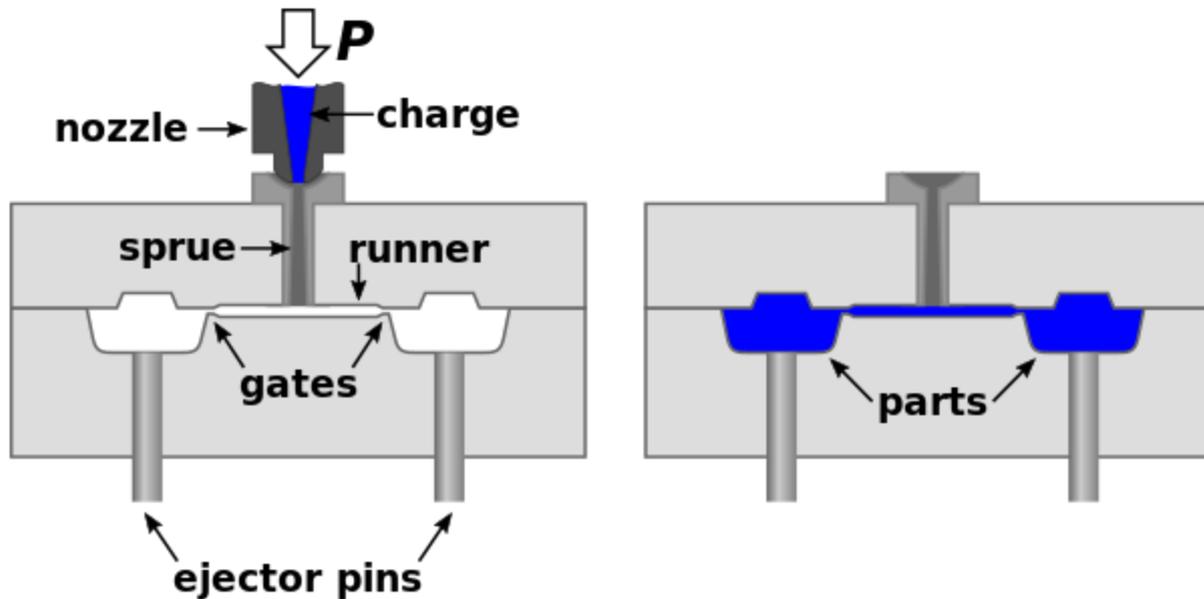
## ❑ Formulation example

Whiteware		Technical Ceramics	
Material	Concentration (vol.%)	Material	Concentration (vol.%)
Kaolin	16	Alumina	45-50
Ball clay	16	Water	40-45
Quartz	16	Ammonium polyacrylate (dispersant)	1-2
Feldspar	16	Methyl cellulose (binder)	5
Water	36	Glycerin (plasticizer)	1
CaCl <sub>2</sub>	<1	Ammonium stearate (lubricant)	1

Rahaman (2003), 391-399

# Injection Molding (1)

- Injection of thick ceramic powder paste with plastic behavior into mold to shape it



"Injection molding diagram" by ariel cornejo - Own work. Licensed under CC BY-SA 4.0 via Commons - [https://commons.wikimedia.org/wiki/File:Injection\\_molding\\_diagram.svg#/media/File:Injection\\_molding\\_diagram.svg](https://commons.wikimedia.org/wiki/File:Injection_molding_diagram.svg#/media/File:Injection_molding_diagram.svg)

## □ Application

Production of high volume, small ceramic articles with complex shapes

# Injection Molding (2)

## □ Example formulation

- Binder content generally higher than (e.g., double or even triple) other ceramic processing method (e.g., slip casting) to ensure plasticity

Component	Formulation 1	Formulation 2
Powder	1 $\mu\text{m}$ alumina, 85 wt.%	20 $\mu\text{m}$ silicon?, 82 wt.%
Major binder	Paraffin wax, 14 wt.%	Polypropylene, 12 wt.%
Minor binder		Microcrystalline wax, 4 wt.%
Other additives	Oleic acid, 1 wt.%	Stearic acid, 1 wt.%

## □ Limited industrial application of injection molding in ceramics

- High tooling cost
- High polymer content (often  $>\sim 10$  wt% or  $\sim 30$  vol%) necessary for injection molding makes the organics removal process more difficult
- Much more complicated than injection molding of polymers due to higher density, viscosity, modulus, and thermal conductivity, but lower fracture toughness

# Drying (1)

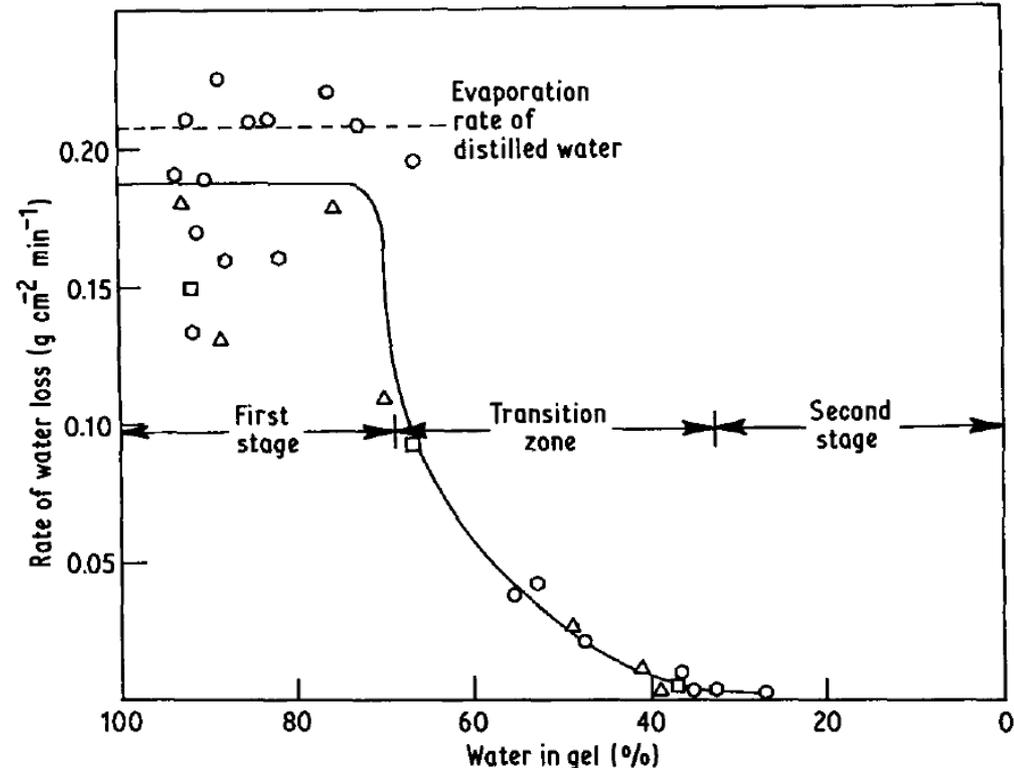
## ❑ Casted or plastically formed parts need to be dried before subsequent binder removal and sintering

Casted or extruded body typically contain moisture of 20-35% by weight, and the more solvent, the greater shrinkage in drying

## ❑ Multi-stage drying

- Constant rate period (CRP)
  - Liquid covers (almost) entire surface
  - Powder compact shrinks in overall size due to capillary compression exerted by liquid
- Falling rate period (FRP)
  - No further reduction in compact size due to particles close touching
  - Gradual decreasing evaporation rate

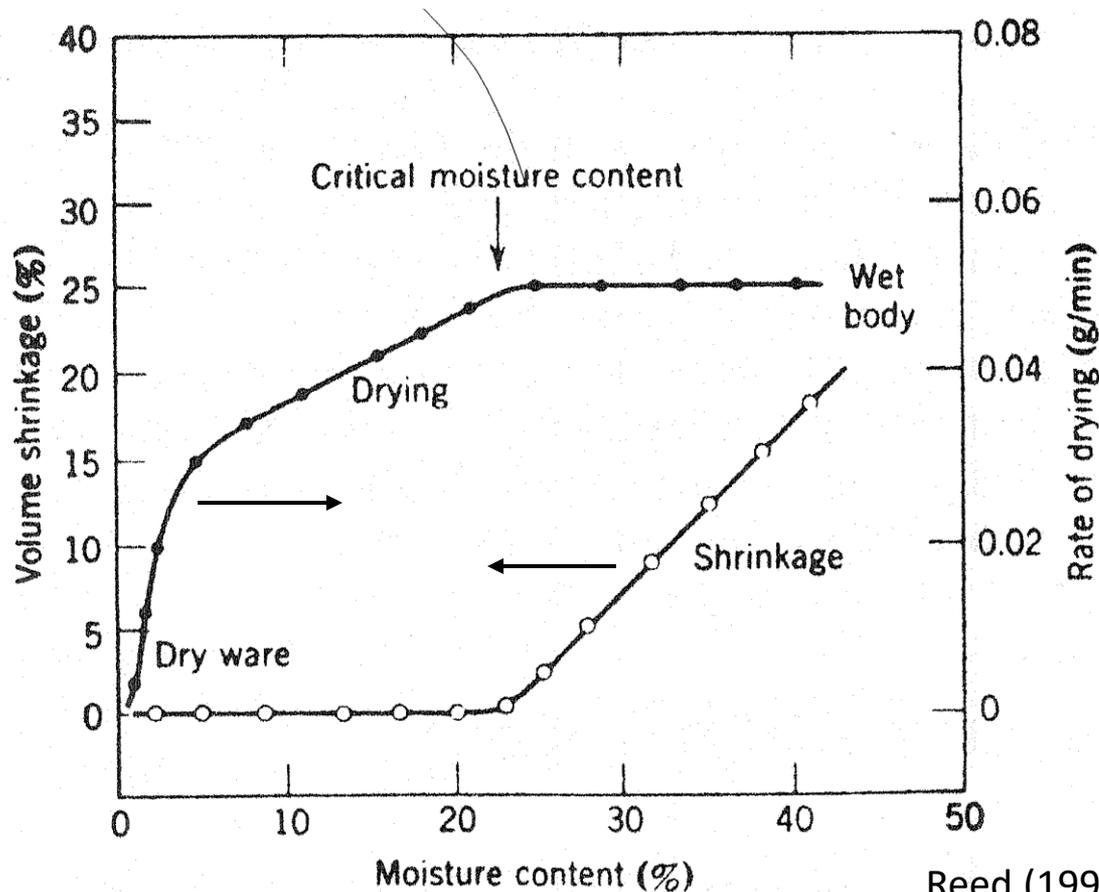
Drying of alumina gel



# Drying (2)

## □ Drying shrinkage

- Large when the solvent content is larger than ~20 wt. %
- Small when the solvent content is less than ~20 wt. %



Reed (1995), 549-558

# Drying (3)

## □ Complications

Capillary action in drying, which, if not controlled properly, may lead to non-uniformity and even cracking

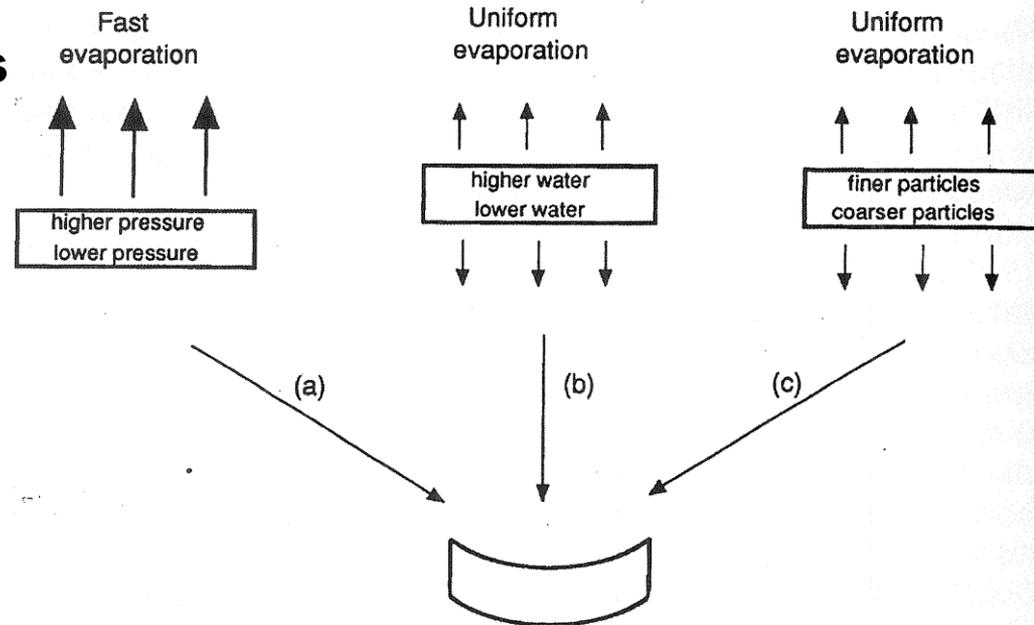
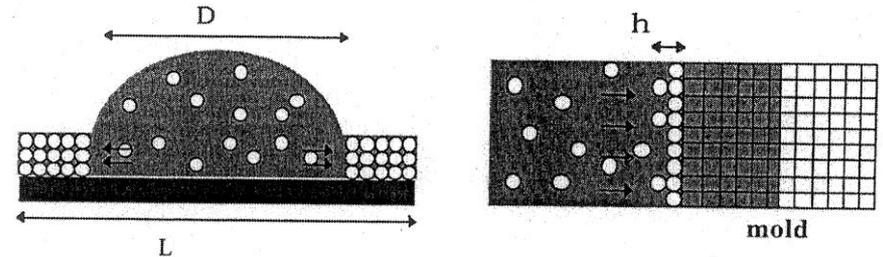
## □ Drying defects

- Deformation such as bending
- Crack formation

## □ Ways to mitigate drying defects

- Increase drying time: even days for large body in production
- Increase particle size - not too practical
- Increase drying temperature (which decreases viscosity) while maintaining high humidity (for water as solvent)

Schematics illustrate drying or solvent removal over semi-dried powder compact



Rahaman (2003), 405-410

# Binder Removal

## □ Ways of binder removal

- Capillary flow
  - Green body placed in powder bed or a porous substrate that absorbs the melted binder
- Solvent extraction
  - Used to remove the soluble component of the binder system
- **Thermal debinding**
  - Stage 1: Softening of binder at temperature of ~150-200 °C
  - Stage 2: Thermal degradation of the polymer binder by breaking into smaller molecules or, when oxygen is present, oxidation into smaller molecules at ~200-400 °C
  - Stage 3: Remaining binder removal at > ~400 °C
- Combined method

## □ Practical thermal debinding

- Less critical if binder volume content < 5 vol.%
- Critical for tape casted or extruded body with much higher binder content
- Need balance between binder removal rate and avoidance of structural defects – sometimes debinding take days to finish
- Generally debinding at slightly lower temperature in oxidizing atmosphere than in inert atmosphere

Rahaman (2003), 409-418



# Green Body Characterization

- ❑ **Green body quality determines, to a large extent, the quality of sintered ceramics**
- ❑ **Characterization of green body**
  - Relative density or porosity
    - Dimension-weight measurement for regular sample (e.g., pellet)
  - Pore size distribution
    - Mercury porosimetry
    - SEM and associated image analysis
  - Other techniques
    - Impregnation with polymers (low viscosity epoxy or MMA monomer followed by hardening to secure the structure) followed by cross-sectioning and image analysis

# Homework

□ For the plots below for random packing of bi-model sphere mixtures (one large sphere and one small sphere), explain with simple calculation why the highest packing density reachable is  $\sim 0.86$  and also estimate the weight fraction of coarse sphere within the total bi-model sphere mixtures when the system reaches the highest packing density

Rahaman (2003),  
p. 334-337  
Plots original data from  
McGeary, J Am Ceram  
Soc, 1961 vol. 44, p513

